

## NOTATION

$R$  = pipe radius  
 $T$  = local time-averaged temperature  
 $T_c$  =  $T$  at pipe center  
 $y$  = radial distance from wall

## Greek Letters

$\epsilon$  = eddy viscosity  
 $\epsilon_H$  = eddy diffusivity for heat  
 $\phi$  =  $(T - T_c)_{\text{calc}} / (T - T_c)_{\text{exp}}$

## Subscripts

calc = calculated  
exp = experimental

## LITERATURE CITED

- Azer, N. Z., and B. T. Chao, "A mechanism of turbulent heat transfer in liquid metals," *Intern. J. Heat Mass Transfer*, **1**, 121 (1960).  
Brinkworth, B. J., and P. C. Smith, "Velocity distribution in the core of turbulent pipe flow," *Chem. Eng. Sci.*, **24**, 787 (1969).

- Buhr, H. O., A. D. Carr, and R. E. Balzhiser, "Temperature profiles in liquid metals and the effect of superimposed free convection in turbulent flow," *Intern. J. Heat Mass Transfer*, **11**, 641 (1968).  
Deissler, R. G., "Analysis of fully developed turbulent heat transfer at low Péclet numbers in smooth tubes with applications to liquid metals," NACA RM E 52FO5 (1952).  
Hughmark, G. A., "Turbulent diffusivities for turbulent pipe flow," *AIChE J.*, **20**, 172 (1974).  
Jenkins, R., "Variation of eddy conductivity with Prandtl modulus and its use in prediction of turbulent heat transfer coefficients," *Heat Transfer and Fluid Mechanics Institute*, pp. 147-158, Stanford Univ. Press, Calif. (1951).  
Notter, R. H., and C. A. Sleicher, "The eddy diffusivity in the turbulent boundary layer near a wall," *Chem. Eng. Sci.*, **26**, 161 (1971).  
———, "A solution to the turbulent Graetz problem—III. Fully developed and entry region heat transfer rates," *ibid.*, **27**, 2073 (1972).  
Sleicher, C. A., A. S. Awad, and R. H. Notter, "Temperature and eddy diffusivity profiles in NaK," *Intern. J. Heat Mass Transfer*, **16**, 1565 (1973).

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## Reply to Notter and Sleicher Note

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The accuracy of the eddy diffusivity ratio for the core region of turbulent pipe flow is related to problems in obtaining both heat and momentum diffusivities. I question that these ratios are more accurate than the 20% maximum deviation shown by the prior R & D note for the core region.

Notter and Sleicher state that the contention of a unity ratio for eddy diffusivities of heat and momentum at all radial positions for fully developed pipe turbulence is unwarranted, is in conflict with theoretical analyses, and will lead to errors in calculated heat transfer rates. My note did not suggest a unity ratio for all radial positions but only for the core. Figure 1 shows data for  $y/R > 0.075$ . Data are not shown for the wall region because

there is an indication that the wall region ratio may not be unity (Hughmark, 1973). The models that yield a diffusivity ratio less than unity for liquid metals are based upon widely differing assumptions and approximations as stated by Notter and Sleicher, thus these do not appear to represent a theoretical analysis of greater accuracy than the broad range of assumptions and approximations. Table 1 shows Nusselt numbers calculated in accordance with Equations (19), (20), and (21) of my paper (1971) and Equation (1) of the note (1972) in comparison to the experimental values reported by Sleicher, Awad, and Notter. Thus these calculated values represent the assumption of an equal diffusivity ratio for the core region. The three high velocity runs show agreement of about 10% which is excellent for liquid metal heat transfer data. The equal diffusivity ratio assumption does not lead to gross error as is implied by Notter and Sleicher.

TABLE 1. NUSSLETT NUMBERS

$Re$	Notter et al. experimental $Nu$	Calculated $Nu$
26,000	6.8	7.9
52,000	9.1	10.4
79,000	10.5	12.8
106,000	13.5	14.8
203,000	20	20.7
302,000	29	31

## LITERATURE CITED

- Hughmark, G. A., "Heat and Mass Transfer for Turbulent Pipe Flow," *AIChE J.*, **17**, 902 (1971).  
———, "Notes on Transfer in Turbulent Pipe Flow," *ibid.*, **18**, 1072 (1972).  
———, "Additional Notes on Transfer in Turbulent Pipe Flow," *ibid.*, **19**, 1054 (1973).